

Composite particles as active catalysts for the SO₃ dissociation reaction of the

thermochemical storage scheme based on elemental sulfur

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INTRODUCTION

The work is in the framework of definition & validation of a novel power cycle via coupling of a centrifugal particle receiver^[1] for solar towers & a compact sulfur-based Thermo-Chemical Storage (TCS) scheme. The concept combines high operating temperatures with high energy density storage (12.5 MJ/kg S) potential.

Endothermic reaction steps (charge)

 $H_2SO_{4(aq)} \rightarrow 2SO_{3(g)} + 2H_2O_{(g)} T = 450-500^{\circ}C$ $2SO_{3(g)} \rightarrow 2SO_{2(g)} + O_{2(g)} T = 700-900^{\circ}C$ $\Delta H = +560 kJ/mol$

Exothermic reaction steps (discharge)

 $2H_2O_{(I)} + 3SO_{2(g)} \rightarrow 2H_2SO_{4(aq)} + S_{(s)}T = 50-200^{\circ}C \Delta H = -260 kJ/mol$ $S_{(I)} + O_{2(g)} \rightarrow SO_{2(g)} T = 500-1500^{\circ}C \Delta H = -300 kJ/mol$



The present work focuses on the development and experimental evaluation of oxide-based particles as both catalysts for the SO₃ dissociation reaction (primarily) and Heat Transfer Fluid (HTF). Main requirements are high thermo-mechanical strength, resistance to chemically harsh environment & suitable particle color. The study includes structural, morphological, mechanical & catalytic activity results.

STRUCTURAL, MORPHOLOGICAL & MECHANICAL PROPERTIES

Structural characterization by X-Ray Diffraction

Mechanical strength by Crushing Strength (CS) measurements

	Material	T _{calcination} /°C	Phases identified	Cs _{fresh} /N	
APTL	Commercial Fe ₂ O ₃	950	Fe ₂ O ₃	22.8	
	Commercial Fe ₂ O ₃	1200	Fe ₂ O ₃	70.7	
	CommFe ₂ O ₃ /clay=75/25	950	Fe ₂ O ₃ , SiO ₂	2.5	
	CommFe ₂ O ₃ /clay=75/25	1200	Fe ₂ O ₃ , SiO ₂	35.0	
	Mill-scale (Ind)	950	Fe ₂ O ₃ , SiO ₂	3.5	
	Mill-scale (Ind)	1200	Fe ₂ O ₃ , SiO ₂	13.2	
	IndFe ₂ O ₃ /clay=75/25	950	Fe ₂ O ₃	11.7	
	IndFe ₂ O ₃ /clay=75/25	1200	Fe ₂ O ₃	107.5	
	Clay	900	SiO ₂ , Al ₂ O ₃ , Al ₂ SiO ₅	14.1	
Baltic Ceramics (BCR)	BCR_1_425_850		Al_2O_3 , traces of FeTi ₂ O ₅ , Fe ₂ O ₃ , Mn ₂ O ₃		
	BCR_2_425_850		Al ₂ O ₃ , Al ₂ (Al _{2.5} Si _{1.5})O _{9.75} , traces of FeTi ₂ O ₅ , Fe ₂ O ₃ , Mn ₂ O ₃		
	BCR_2_850_1180	1280	same composition as BCR_2_425_850		
	BCR_3_425_850		Al ₂ O ₃ , traces of FeTi ₂ O ₅	>100	
	BCR_4_425_850		Al ₂ O ₃ , traces of FeTi ₂ O ₅ , Fe ₂ O ₃		
	BCR_4_850_1180		same composition as BCR_4_425_850		
	BCR_5_841_1680	A	Al_2O_3 , SiO ₂ , traces of Fe ₂ O ₃ , 3Al ₂ O ₃ ·2SiO ₂		

Morphological characterization via SEM



Near spherical; size range 425-1680 μm (BCR), 700-1400 μm (APTL)

APTL samples:

- Low crystallinity & absence of clear Al₂O₃ & Al-Si-O peaks
- Higher calcination temperature \rightarrow more sintered structures & improved $CS \rightarrow$ Improved structural stability
- Major elements (EDS): Fe, Al, Si
- BET showed low surface area & no porosity (Hg-porosimetry)

BCR samples:

- Bauxite-based proppants with main phases: Al_2O_3 & aluminosilicates. Small amounts of Fe₂O₃, Mn₂O₃ & FeTi₂O₅
 - SEM results for same particle size (425-850 µm) very similar
 - ✓ Major elements (EDS): Al, Mn, Si. Also present Ca, Ti & Fe
 - Negligible surface area (BET) & no porosity





After test

CATALYTIC ACTIVITY EVALUATION SO₃ conversion %

blank

ersion / 20 20

10

SO₂ analysis by UV-Vis spectrometry in a setup for catalytic activity measurements

- On-stream exposure duration per test: 60 min
- Temperature: 850°C; Pressure: 1 bar \bullet
- Feed: concentrated sulfuric acid (98%), 0.12 ml/min
- Catalyst quantity per test: 1 g

	Material	SO ₃ conversion/%	Particle Color	CS _{after exp.} /N
	Commercial Fe ₂ O ₃ _950	53.6	dark red-blackish	29.0
	Commercial Fe ₂ O ₃ _1200	8.0	blackish-black	74.9
	CommFe ₂ O ₃ /clay=75/25_950	55.1	medium red	8.6
F	CommFe ₂ O ₃ /clay=75/25_1200	44.4	dark red-blackish	33.4
0 <	Mill-scale (Ind)_950	40.0	dark brown-blackish	7.3
	Mill-scale (Ind)_1200	36.8	blackish	12.9
	IndFe ₂ O ₃ /clay=75/25_1200	23.0	blackish	71.9
	Clay_900	15.4	light yellow	5.6
	BCR_1_425_850	10.3	black	61.3
	BCR_2_425_850	13.6	black	42.7
	BCR_2_850_1180	15.5	blackish	50.2
	BCR_3_425_850	9.9	blackish	52.0
	BCR_4_425_850	5.0	black	52.9
	BCR 4 850 1180	4.1	black	57.9

Commercial Fe2O3_950 CommFe2O3/clay=75/25_1200 IndFe2O3/clay=75/25_1200 140 Commercial Fe2O3_950 BCR 2 425 850 BCR 2 850 1180 BCR 5 841 1680 equilibrium CommFe2O3/clay=75/25 1200 120 IndFe2O3/clay=75/25_1200 z BCR 2 425 850 **1**00 BCR_2_850_1180 strength BCR 5_841_1680 80 60 Crushing 40

Indicative comparative results of SO₃ conversion and CS measurements

- APTL particles rich in Fe₂O₃ high efficiency
 - Samples calcined at 950°C more active cf. the ones calcined at 1200°C, but lower structural stability
 - Sintering at 1200°C detrimental to catalytic activity
 - Stable CS values before & after testing for selected samples
- BCR proppants relatively low performance
 - Absence or low content of catalytically active phases
 - No significant effect of particle size
 - CS reduced by >50% after 60 min of exposure \rightarrow but still high

Mechanical properties evaluation

Fresh

BCR_5_841_1680

13.4

47.7

blackish

- Equilibrium 81%
- Blank conversion 5%

CONCLUSIONS

- \checkmark Extremely high mechanical integrity leads to low catalytic activity in the BCR proppants \rightarrow lack of sufficient catalytically active phases + no porosity
- CommFe₂O₃/clay=75/25_1200 most promising material so far \rightarrow combines SO₃ conversion >40%, CS > 20 N & dark color \rightarrow Further improvement to be closer to s.o.a. performance ^{[2],[3]}

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Combination of both approaches to create modified proppants relatively rich in catalytically active phases (e.g. Fe₂O₃, CuO) and high mechanical integrity Preliminary results on CuO-containing BCR proppants showed SO₃ conversion >50%

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